

أرامكو السعودية soudi oromco Exposure of various polymer lined carbon steel pipe section to a sour HC fluid at maximum service temperature: Methodology and Observations

### subsea 7

Maria Eleni Mitzithra TWI Ltd

> JOINING INNOVATION AND EXPERTISE

Anwar Parvez Abdulaziz Asiri (Saudi Aramco)

Colin Jones James Taylor (Subsea 7)

Bernadette Craster Barnaby King (TWI Ltd)

Marine Corrosion Forum January 2021

# Polymeric liners used for:

- Water conveyancing
  (on land and subsea water injection pipelines)
- ~20yrs in producing wellbores as lining for tubulars
- Chemical production plants

Increasing interest to use in:

- Subsea pipeline rehabilitation
- Sour hydrocarbon conveyancing

## **Overview and Objectives**



Establish the condition of X52 lined with a thermoplastic via flow loop testing in sour environment:

- Degree of alteration of 4 polymeric liners
- Surface condition of carbon steel under liner

## Test material



- A total length of 914mm with approx. 500mm lined pipe.
- 4 Liners (10-11mm thick):
  - Polyamide (Type 1 and 2)
  - PE-RT
  - PVDF



### Test material prior to exposure







- X52 steel rated for sour service.
- Features due to manufacturing process and/or post manufacturing atmospheric exposure.
- Evidence of de-carburisation

# The flow loop



# Test conditions

Material	Test temperature (°C)	Test pressure (barg)	Duration at test temperature (days)	
PA type 1	80			
PA type 2	90	89	180	
PE-RT	90			
PVDF	130		180	

- Sour hydrocarbon fluid (ISO 23936-1:2009)
- Displacement rate of fluid: 5m/sec.
- Static period at 130°C for PVDF.
- Depressurisation at 70barg min<sup>-1</sup> at 90 and 180days.

## Sections after exposure



- Polymeric liner turned over for a view of the interfacial transition zone
- Visual observations made of liner and carbon steel surface
- Polymer sectioned for mechanical, permeability, calorimetric and spectroscopic comparison with unaged liners
- Carbon steel surface and bulk examined for cracking and corrosion using ultrasound, diffraction and microscopy

## Properties of the tested polymeric liner

#### Permeability coefficients from dry gas mixture



# Properties of the tested polymeric liner

Material	Liner thickness (nominal, mm)	Colour	Enthalpy of Melt J g <sup>-1</sup>	Melting point °C	Young's Modulus GPa (at test temperature)
PA type 1 (unaged)	10.8	Yellow	42	178	0.36 (80°C)
PA type 1	11.4	Black	46	178	0.41(80°C)
PA type 2 (unaged)	10.5	Black	31	193	0.26(90°C)
PA type 2	11.3	Black	39	196	0.34(90°C)
PE-RT (unaged)	10.8	Black	146	133	0.12(90°C)
PE-RT	12.2	Black	150	134	0.11(90°C)
PVDF (unaged)	10.5	White	48	170	0.12(130°C)
PVDF	11.3	Brown	46	168	0.16(130°C)

# Surface morphology of CS test material



### Pitting on CS test material

Under PA Type 1



Under PA type 2







Under PVDF



Unlined



- Near ventilation

   Image: state s
- D0000000 1074 + 4010 pg
  - Near ventilation



- Unlined the most affected.
- PA type 1 and PVDF lined sections the least affected.
  - Change in pit shape + corrosion scaling  $\rightarrow$ Wet sour corrosive environment at the CS-liner interface.
  - Role of pre-existing flaws.

# Corrosion scaling on CS test material



 $\Box$  Magnetite (Fe<sub>3</sub>O<sub>4</sub>) adjacent to the steel



□ Mackinawite (Fe<sub>1+x</sub>S) □ Initial stage of exposure





Pyrrhotite (Fe<sub>1-x</sub>S), Pyrite (FeS<sub>2</sub>) Retardation of corrosion rate



Under PVDF







Unlined





Near ventilation





# Conclusions

- Condition of test material after 180 days at and above 80°C & 89 bar:
- Surface morphology (pitting & scaling thickness) of CS:
  - Corrosion resistance:

PVDF>PA Type 2>PA Type 1> PE-RT>Bare carbon steel.

- Iron sulfides acknowledged for their protective natures.
- □ Condition of the polymeric liners:
  - No collapse during rapid gas decompression events.
  - No substantial alteration in mechanical properties or crystallinity.
  - Swelling but no residual relaxation
  - Loss of additives, present at the 'interfacial' environment.

### Future work

Laboratory and field tests of longer duration (1 year+) for:

- **Quantitative corrosion rates and online NDT monitoring?**
- □ Vapour permeation through the liner vs. time and level of condensation at the interface?
- Critical scale thickness (vs annular space) for eventual liner collapse?
- H<sub>2</sub>S-containing brine & chloride permeation through the liner vs. time?
- □ Use of higher strength low alloy steel, x65 or X70? Hydrogen behind the liner vs. SSC?
- Presence of girth welds?

### Thank you for your attention. Any questions? NACE CORROSION 2020 Digital proceedings Paper no. C2020-14821

David Smyth Boyle Edward Watts Phil Robinson James Redman Ian Wallis Harry Froment Sheila Stevens Sally Day Diane Shaw Catherine Richardson

# Polymeric material swaged but not exposed

Material	Liner thickness (nominal, mm)	Colour	Enthalpy of Melt J g <sup>-1</sup>	Melting point °C	Young's Modulus GPa (at test temperature)
PA type 1	10.8	Yellow	42	178	0.36 (80°C)
PA type 2	10.5	Black	31	193	0.26(90°C)
PE-RT	10.8	Black	146	133	0.12(90°C)
PVDF	10.5	White	48	170	0.12(130°C)

Material	Temperature (°C)	Permeability (K)			
		10 <sup>-7</sup> cm <sup>2</sup> s <sup>-1</sup> bar <sup>-1</sup>			
		CO <sub>2</sub>	CH <sub>4</sub>	$H_2S$	
PA type 1	80	0.4	0.1	1.1	
PA type 2	90	0.6	0.2	1.5	
PE-RT	90	2.3	1.2	4.4	
PVDF	130	3.0	0.7	3.3	

Steady state flux through the liner after approximately 112 days. Experiments on dry gas supply.